

Detail Modeling of Melt Layer Splashing and Erosion Losses of PFC

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Outline

- Brief Introduction
- Our Previous Work
- Viscous Linear Analysis with Heat & Mass Transfer
- CFD Modelling
- Summary





Melt Layer Erosion Mechanisms

□ Macroscopic losses of melt layer during plasma disruptions is a *serious concern* because its thickness can be two orders of magnitude higher than vaporization thickness

- Two main mechanisms of melt layer losses suggested:
- Development and growth of *hydrodynamic instabilities* due to various forces on the melt surface resulting in liquid droplets that are carried away by the plasma wind
- Boiling with vapor bubble bursting at the melt surface and formation of jet-droplets

□ Amount of lost melt is uncertain depending on disrupting plasma parameters, deposited energy flux, melt properties, design, etc.



Examples of Macroscopic Melt Splashing







TEXTOR: Sergienko et al.,
 MK-200: Safronov et al.,
 MK-200: Safronov et al.,

 Phys. Scr. T128 (2007) 81
 PAST 8 (2002) 27
 F

QSPA-T: Bazylev et al., Fusion Eng. Des. 84 (2009) 441



QSPA Kh-50: Garkusha et al., J. Nucl. Mater. 390 (2009) 814



VIKA: Litunovsky et al., Fusion Eng. Des. 49 (2000) 249



Melt Layer Spraying and Splashing in TEXTOR



Coenen et al., J. Nucl. Mater. 415 (2011) S78; Coenen et al., Nucl. Fusion 51 (2011) 083008; Nucl. Fusion 51 (2011) 113020.





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Erosion due to Vaporization & Melting



 \Box Tungsten erosion due to vaporization ~ 1-2 μm

- **□** Melt layer thickness ~200 µm at 1.0 ms
- □ Melt boiling can take place

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Hassanein & Konkashbaev J. Nucl. Mater. 233 (1996) 713



K-H Instability of Inviscid Plasma-Tungsten Melt



Two-Fluid Computational Model

□ Volume of Fluid method → plasma & melt are pure, inviscid immiscible fluids with volume fractions $\alpha_p + \alpha_m = 1$



- □ Gravity and surface tension effects are included as source
- Modeling performed using FLUENT package



Computational Modeling of Plasma-Melt Flow

Plasma-liquid interface perturbed with most unstable wavelength predicted by the linear stability analysis, ~2 mm

1.00e+00 9.50e-01

9.00e-01 8.50e-01 8.00e-01

7.50e-01 7.00e-01 6.50e-01 6.00e-01

5.50e-01

5.00e-01 4.50e-01

4.00e-01 3.50e-01 3.00e-01



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> at ~0.4 μ s, small liquid tungsten plumes ~2 mm at the wave crests

> at ~1 μ s, elongated liquid tungsten ligaments penetrating into the plasma

 \rightarrow at ~2-4 µs, lengthening, thinning, and collisions of melt ligaments with capture of small pockets of the plasma

> at > 6 μ s, highly irregular topological structures of liquid tungsten patterns with breaks and holes





Computational Modeling of Plasma-Melt Flow



^{1.00e+00} ^{9.50e-01} ^{9.00e-01} ^{8.00e-01} ^{8.00e-01} with shorter wavelength, ~0.5 mm

source tension force

^{200e01} > growing of new waves with most
 ^{100e01} dangerous wavelengths in agreement with predictions from the linear stability analysis

 \succ development of ligaments penetrating into the plasma, splitting the bulk of a melt layer, ligament collisions and coalescence, thinning and breaking into droplets

Miloshevsky & Hassanein, Nucl. Fusion 50 (2010) 115005; J. Nucl. Mater. 415 (2011) S74.

6.50e-01

3.00e-01

2.50e-01



Bubble Growth, Vaporization, and Melt Loss due to Incident Plasma Wind



- Another mechanisms of melt-layer loss is volume bubble boiling due to overheating of melt layer
- Bubbles can grow, reach liquid surface, and then burst. Bursting bubble forms a jet. The jet is then disintegrates into droplets
- □ The melt erosion has a form of a splashing wave. The liquid droplets are then carried away by the incident plasma stream wave.

PURDUE UNIVERSITY Hassanein et al. J. Nucl. Mater. 241 (1997) 288

CFD Simulations of Erosion due to Boiling and Bubble Bursting with Ejection of Jet-Droplets



□ CFD showed formation of jets and breakage into droplets

Amount of jet-droplets was integrated into moving boundary model
 Final erosion from boiling depends on many parameters and uncertain

13

Y. Shi, G. V. Miloshevsky & A. Hassanein. Boiling induced macroscopic erosion of plasma facing components in fusion devices. Fusion Eng. Des. 86 (2011) 155-162.

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Instability of Viscous Potential Plasma-Melt Flow Critical Velocity & Growth Rate:

Viscous Potential Flow:

$$\Delta V > \sqrt{\frac{(\mu'_{m} + \mu'_{p})^{2}}{\rho'_{m} \mu'_{p}^{2} + \rho'_{p} \mu'_{m}^{2}}} \left(\frac{g(\rho_{m} - \rho_{p})}{k} + (\gamma + \gamma_{H})k\right)$$

$$\sigma_{R} = \pm \sqrt{\frac{k^{2}(\rho'_{m} \mu'_{p}^{2} + \rho'_{p} \mu'_{m}^{2})}{(\mu'_{m} + \mu'_{p})^{2}(\rho'_{m} + \rho'_{p})}} \Delta V^{2} - \left(kg \frac{\rho_{m} - \rho_{p}}{\rho'_{m} + \rho'_{p}} + \frac{k^{3}(\gamma + \gamma_{H})}{\rho'_{m} + \rho'_{p}}\right)$$

$$if \frac{\mu'_{p}}{\mu'_{m}} = \frac{\rho'_{p}}{\rho'_{m}} \implies \mu_{p} \to 0 \qquad r = \rho_{p} / \rho_{m} \sim \mu_{p} / \mu_{p}$$

Inviscid Potential Flow:

$$\Delta V > \sqrt{\frac{\rho_m' + \rho_p'}{\rho_m' \rho_p'}} \left(\frac{g(\rho_m - \rho_p)}{k} + (\gamma + \gamma_H)k \right)$$

$$\sqrt{\frac{k^2 \rho_p' \rho_p'}{k}} \left(\frac{g(\rho_m - \rho_p)}{k} + (\gamma - \gamma_H)k \right)$$

$$\sigma_{R} = \pm \sqrt{\frac{k^{-} \rho_{m} \rho_{p}}{(\rho_{m}' + \rho_{p}')^{2}}} \Delta V^{2} - \left(kg \frac{\rho_{m} - \rho_{p}}{\rho_{m}' + \rho_{p}'} + \frac{k^{3} (\gamma + \gamma_{H})}{\rho_{m}' + \rho_{p}'}\right)$$

 $r = \rho_p / \rho_m \sim 10^{-10}$ $n = \mu_p / \mu_m \sim 10^{-3}$ r << nlow viscosity case

Funada & Joseph, J. Fluid Mech. 445 (2001) 263-283 $V^{URDU_{e}}$ $V^{URDU_{e}}$



Melt Erosion from Capillary Droplet Ejection Model



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Instability of Viscous Potential Plasma-Melt Flow

Effects of Mass & Heat Transfer Across the Interface

$$\Delta V > \sqrt{\frac{2(\delta(\coth(kh_m) + \coth(kh_p)) + 2k^2(\mu'_m + \mu'_p))^2 \times}{\delta^2(\rho'_p \coth^2(kh_m) + \rho'_m \coth^2(kh_p)) + 4k^4(\rho'_m \mu'_p^2 + \rho'_p \mu'_m^2) + }}}$$

$$S = \frac{F}{L} \left(\frac{1}{h_m} + \frac{1}{h_p} \right)$$

$$S = \frac{1}{h_m} \left(\frac{1}{h_m} + \frac{1}{h_m}$$

Instability of Viscous Potential Plasma-Melt Flow

Effects of Mass & Heat Transfer Across the Interface



19



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Open Field Operation and Manipulation (OpenFOAM) is Open Source CFD Toolbox with extensive multi-physics capabilities

> Numerous pre-configured finite volume solvers, utilities, and libraries that are written in C++ and under active development with capabilities of commercial CFD software

> 2D or 3D structured/unstructured mesh and parallel running

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> Possibility for users to extend and implement new physics models: existing solvers can be used as templates for further development

> Representation of partial differential equations through natural language of equation mimicking: $\int_{C}^{\text{solve}} dt$

Volume of Fluid (VOF) Model available in OpenFOAM:

two immiscible & isothermal fluids

 $\frac{\partial \rho \vec{u}}{\partial t} + \nabla \cdot (\rho \vec{u} \vec{u}) = -\nabla p + \nabla \cdot (\mu (\nabla \vec{u} + (\nabla \vec{u})^T)) + \sigma \kappa \nabla \alpha_m + \rho \vec{g} - \text{momentum}$

$$\frac{\partial \alpha_m}{\partial t} + \nabla \cdot (\alpha_m \vec{u}) + \nabla \cdot (\alpha_m (1 - \alpha_m) \vec{u}_c) = 0 \quad \text{-volume fraction}$$

 $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{u}) = 0 \quad \text{- continuity}$

$$\rho = \alpha_m \rho_m + \alpha_p \rho_p \qquad \mu = \alpha_m \mu_m + \alpha_p \mu_p \qquad \alpha_p = 1 - \alpha_m$$
$$\rho_j = \rho_{0j} + \psi_j (p - p_{0j}), \quad j = m, p$$



Implementation of Heat & Mass Transfer Models in VOF Model: $\frac{\partial \rho \vec{u}}{\partial t} + \nabla \cdot (\rho \vec{u} \vec{u}) = -\nabla p + \nabla \cdot (\mu (\nabla \vec{u} + (\nabla \vec{u})^T)) + \sigma \kappa \nabla \alpha_m + \rho \vec{g} - \text{momentum}$ $\frac{\partial \alpha_m}{\partial t} + \nabla \cdot (\alpha_m \vec{u}) + \nabla \cdot (\alpha_m (1 - \alpha_m) \vec{u}_c) = \frac{\vec{m}}{\rho} \quad \text{-volume fraction}$ $\frac{\partial \rho c_p T}{\partial t} + \nabla \cdot (\rho c_p \vec{u} T) = \nabla \cdot (K \nabla T) + \dot{h} \quad \text{- heat conduction} \quad \frac{c_p = \alpha_m c_{pm} + \alpha_p c_{pp}}{K = \alpha_m K_m + \alpha_p K_p}$ $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{u}) = \vec{m} \quad \text{continuity} \quad \rho = \alpha_m \rho_m + \alpha_p \rho_p \quad \mu = \alpha_m \mu_m + \alpha_p \mu_p$ $\rho_j = \rho_{0j} + \psi_j (p - p_{0j}) - \zeta_j (T - T_{0j}), \quad j = m, p \quad \alpha_p = 1 - \alpha_m$ Hardt evaporation model: $\dot{m} = (T_i - T_s) N \alpha_m \nabla \alpha_m / (R_{mp}L)$ with $R_{mp} = (2 - \chi) T_s^{3/2} \sqrt{2\pi R_p} / (2\chi L^2 \rho_p)$ and $\dot{h} = L\dot{m}$ Hardt & Wondra, J. Comput. Phys. 227 (2008) 5871 IVERSIT

Effects of Viscous & Thermal Stresses

Plasma-liquid interface perturbed with 10, 20 & 40 wavelengths (wavelength: 500 μm, 250 μm & 125 μm):



Movie of plasma-liquid interface perturbed with 10 wavelengths (wavelength: 500 µm):





Movie of plasma-liquid interface perturbed with 20 wavelengths (wavelength: 250 µm):





Movie of plasma-liquid interface perturbed with 40 wavelengths (wavelength: 125 µm):





Stabilizing Effect of Mass & Heat Transfer Across the Interface

Plasma-liquid interface perturbed with 50 wavelengths (100 µm):



Movie of plasma-liquid interface perturbed with 50 wavelengths (wavelength: 100 µm):





Summary

- Plasma instabilities have serious effects on PFCs and should be significantly minimized or totally mitigated
- Melt layer erosion can substantially reduce lifetime and contaminate the plasma
- □ Viscous forces have strong destabilizing effects on melt layer: reduced critical velocity & wavelength of fasters growing waves
- Phase change with intense vaporization stabilizes short-length waves suppressing the growth of viscous instability
- When Vaporization is insignificant → growth of short-length waves, their transformation into ligaments, fine melt droplets from ligament tips, droplet collisions and drag by plasma flow



Reserved Slides







 $T_w = 383.15 K$

Analytical solution:

Model parameters:

$$x_{i}(t) = 2\beta\sqrt{k_{v}t} \qquad \lambda_{v} = 10^{-2} \div 10^{-1} W/(m K) \quad \lambda_{l} = 1W/(m K)$$

$$T(x,t) = T_{w} + \frac{T_{sat} - T_{w}}{erf(\beta)} erf\left(\frac{x}{2\sqrt{k_{v}t}}\right) \qquad c_{pv} = 10^{3} J/(kg K) \quad c_{pl} = 10^{3} J/(kg K)$$

$$h_{e} = 10^{6} J/kg \qquad \sigma = 10 mN/m$$

$$k_{v} = \frac{\lambda_{v}}{\rho_{v}c_{pv}} \text{ and } \beta \exp(\beta^{2}) = \frac{c_{pv}(T_{w} - T_{sat})}{\sqrt{\pi}h_{e}} \qquad \mu_{v} = 10^{-5} Pa s \quad \mu_{l} = 10^{-2} Pa s$$

$$\rho_{v} = 1 kg/m^{3} \qquad \rho_{l} = 1 kg/m^{3}$$
Hardt & Wondra, J. Comput. Phys. 227 (2008) 5871



Movie of volume fractions of vapor & liquid: $\lambda_v = 0.1 W/(m K)$





Movie of evolution of temperature of vapor & liquid: $\lambda_v = 0.1 W/(m K)$





Plasma impact with velocity 100 km/s in two times larger domain Movie of plasma-liquid interface perturbed with 5 wavelengths:







Phenomenological Capillary Droplet Model Main assumptions:

- extension of linear stability analysis to an essentially non-linear regime
- approximation of a deep melt: dangerous wavelength $\lambda_{\theta} << h_m$
- fine droplets at wave's peaks are dragged away by the plasma wind

Maximum increment coefficient and dangerous wavelength:

 $\Gamma_{\theta} = 2\left(\rho_p \Delta V^2\right)^{3/2} / \left(3\gamma \sqrt{3\rho_m}\right) \text{ and } \lambda_{\theta} = 3\pi\gamma / \left(\rho_p \Delta V^2\right) \text{ with the radius of droplets assumed as } \sim \lambda_{\theta} / 4$

For QSPA-T conditions: heat loads <1.6 MJ/m² during <0.3 ms $V_p \sim 10^5 \ m/s, \ N_p \sim 3.5 \cdot 10^{22} \ m^{-3} \Rightarrow \rho_p \sim 6 \cdot 10^{-5} \ kg/m^3$ $\lambda_{\theta} \sim 40 \ \mu m$; K-H instability time $\tau \sim 1.8 \ \mu s$

For ITER conditions: weak ELMs <2.5 MJ/m² during <0.3 ms $V_p \sim 10^5 \ m/s, N_p \approx 10^{19} - 10^{20} \ m^{-3} \Rightarrow \rho_p \approx 1.7 \cdot (10^{-8} - 10^{-7}) \ kg \ / m^3$

 $\lambda_{\theta} \sim 14 - 1.4 \text{ cm} >> h_m \implies model is not valid!$

Bazylev et al., Fusion Eng. Des. 84 (2009) 441; Bazylev et al., Phys. Scr. T128 (2007) 229; Bazylev & Landman, Problems Atomic Sci. Technol. 13 (2007) 35

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K-H Instability of Inviscid Plasma-Tungsten Melt



denser plasma shifts dangerous wavelength toward shorter waves, growth rate increases thinner melt layers are more stable than thicker ones H aligned with the melt flow suppresses instabilityH perpendicular to the flow has no influence

